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# Mediating oxidative stress enhances $\alpha$ -ionone biosynthesis and strain robustness during process scaling up

Ching-Ning Huang, Xiaohui Lim, Leonard Ong, Chinchin Lim, Xixian Chen\* and Congqiang Zhang\*

## Abstract

**Background:**  $\alpha$ -Ionone is highly valued in cosmetics and perfumery with a global usage of 100–1000 tons per year. Metabolic engineering by microbial fermentation offers a promising way to produce natural (*R*)- $\alpha$ -ionone in a cost-effective manner. Apart from optimizing the metabolic pathways, the approach is also highly dependent on generating a robust strain which retains productivity during the scale-up process. To our knowledge, no study has investigated strain robustness while increasing  $\alpha$ -ionone yield.

**Results:** Built on our previous work, here, we further increased  $\alpha$ -ionone yield to 11.4 mg/L/OD in 1 mL tubes by overexpressing the bottleneck dioxygenase CCD1 and re-engineering the pathway, which is > 65% enhancement as compared to our previously best strain. However, the yield decreased greatly to 2.4 mg/L/OD when tested in 10 mL flasks. Further investigation uncovered an unexpected inhibition that excessive overexpression of CCD1 was accompanied with increased hydrogen peroxide ( $H_2O_2$ ) production. Excessive  $H_2O_2$  broke down lycopene, the precursor to  $\alpha$ -ionone, leading to the decrease in  $\alpha$ -ionone production in flasks. This proved that expressing too much CCD1 can lead to reduced production of  $\alpha$ -ionone, despite CCD1 being the rate-limiting enzyme. Overexpressing the alkyl hydroperoxide reductase (*ahpC/F*) partially solved this issue and improved  $\alpha$ -ionone yield to 5.0 mg/L/OD in flasks by reducing oxidative stress from  $H_2O_2$ . The strain exhibited improved robustness and produced ~700 mg/L in 5L bioreactors, the highest titer reported in the literature.

**Conclusion:** Our study provides an insight on the importance of mediating the oxidative stress to improve strain robustness and microbial production of  $\alpha$ -ionone during scaling up. This new strategy may be inspiring to the biosynthesis of other high-value apocarotenoids such as retinol and crocin, in which oxygenases are also involved.

**Keywords:** Ionone, Apocarotenoids, Carotenoid cleavage dioxygenases (CCDs), Reactive oxygen species (ROSs), Hydrogen peroxide ( $H_2O_2$ ), Alkyl hydroperoxide reductases

## Background

Ionones are a group of natural ketone compounds composed of 13 carbons with a monocyclic terpenoid backbone [1]. They are carotenoid-derived aroma compounds

found at sub-ppm levels in many flowers and fruits (e.g., rose, sweet osmanthus, orris root, and raspberry). Among these,  $\alpha$ -ionone is a high-value aroma (violet-like) and flavor (raspberry and blackberry-like) [2] compound with an extremely low odor threshold (0.4–3.2 ppb) [3] and a high global usage (on a scale of 100–1000 tons per year). Commercial  $\alpha$ -ionone is currently chemically synthesized, as the extremely low levels in natural sources (e.g., 100 tons of raspberries yields merely 1 g of

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$\alpha$ -ionone) makes such extraction commercially unviable [4].

$\alpha$ -Ionone is the oxidative product of  $\alpha$ -carotene or  $\epsilon$ -carotene that is catalyzed by carotenoid cleavage dioxygenases (CCDs) [5]. CCDs can cleave multiple substrates and typically exhibit a high degree of regio-specificity for double bond positions. In a previous study, we designed an *E. coli*-based “plug-n-play” system to produce  $\alpha$ -ionone,  $\beta$ -ionone and retinoids. We fused the carotenoid cleavage dioxygenase 1 (CCD1) from *Osmanthus fragans* (OfCCD1) with thioredoxin (trxA) to form TOfCCD1 for increasing CCD1 enzyme concentration in the pathway to achieve high titers (this strain was named AI\_0000 (Fig. 1)) [4]. Nevertheless,  $\epsilon$ -carotene (the substrate of CCD1) was still not completely converted in the bacterial strain. This limitation might be because of the poor catalytic properties of TOfCCD1 [4]. To address this issue, we applied directed evolution and enzyme fusion to further engineer the TOfCCD1 enzyme. We successfully improved CCD1 activity and further enhanced  $\alpha$ -ionone production, achieving approximately 3.5 mg/L/OD of  $\alpha$ -ionone. [6].

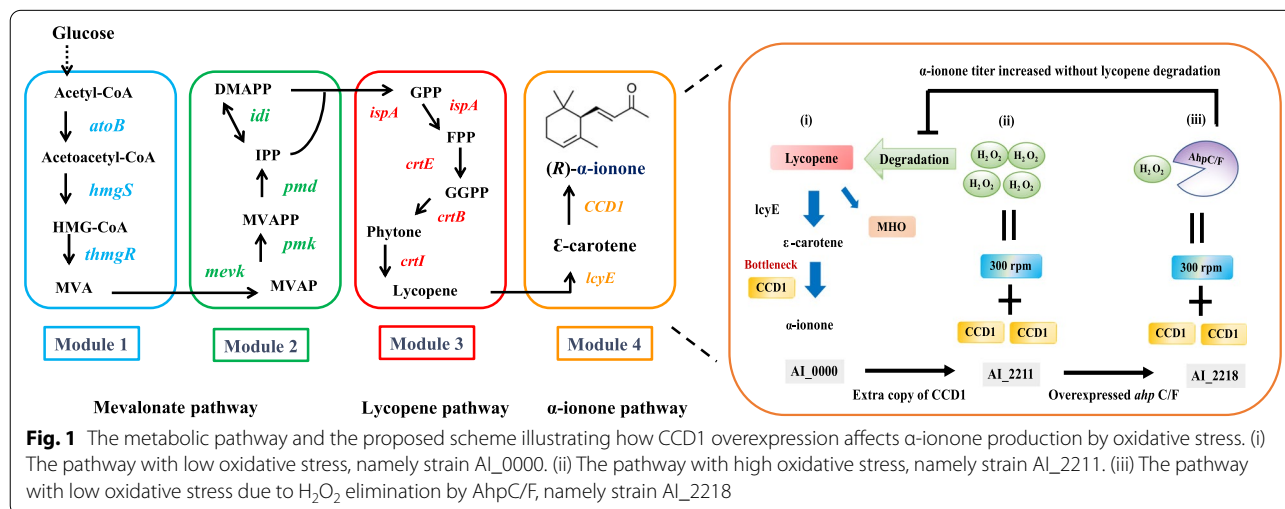
In this study, we further improved the titer of  $\alpha$ -ionone by overexpressing an additional copy of CCD1 on the vector to enhance  $\epsilon$ -carotene conversion to  $\alpha$ -ionone (strain AI\_2211, Fig. 1). However, we found that oxidative stress hindered the ionone production especially for our newly engineered strains when mixing speed was increased during scaling up. This instability severely impacts further scaling up to bioreactors. As oxidative stress is related with reactive oxygen species (ROSs) in *E. coli*, we hypothesized that this phenomenon may be related to the generation of ROSs, particularly hydrogen peroxide ( $H_2O_2$ ). By overexpressing a catalase G (*katG*) or an alkyl hydroperoxide reductase (*ahpC/F*), we found

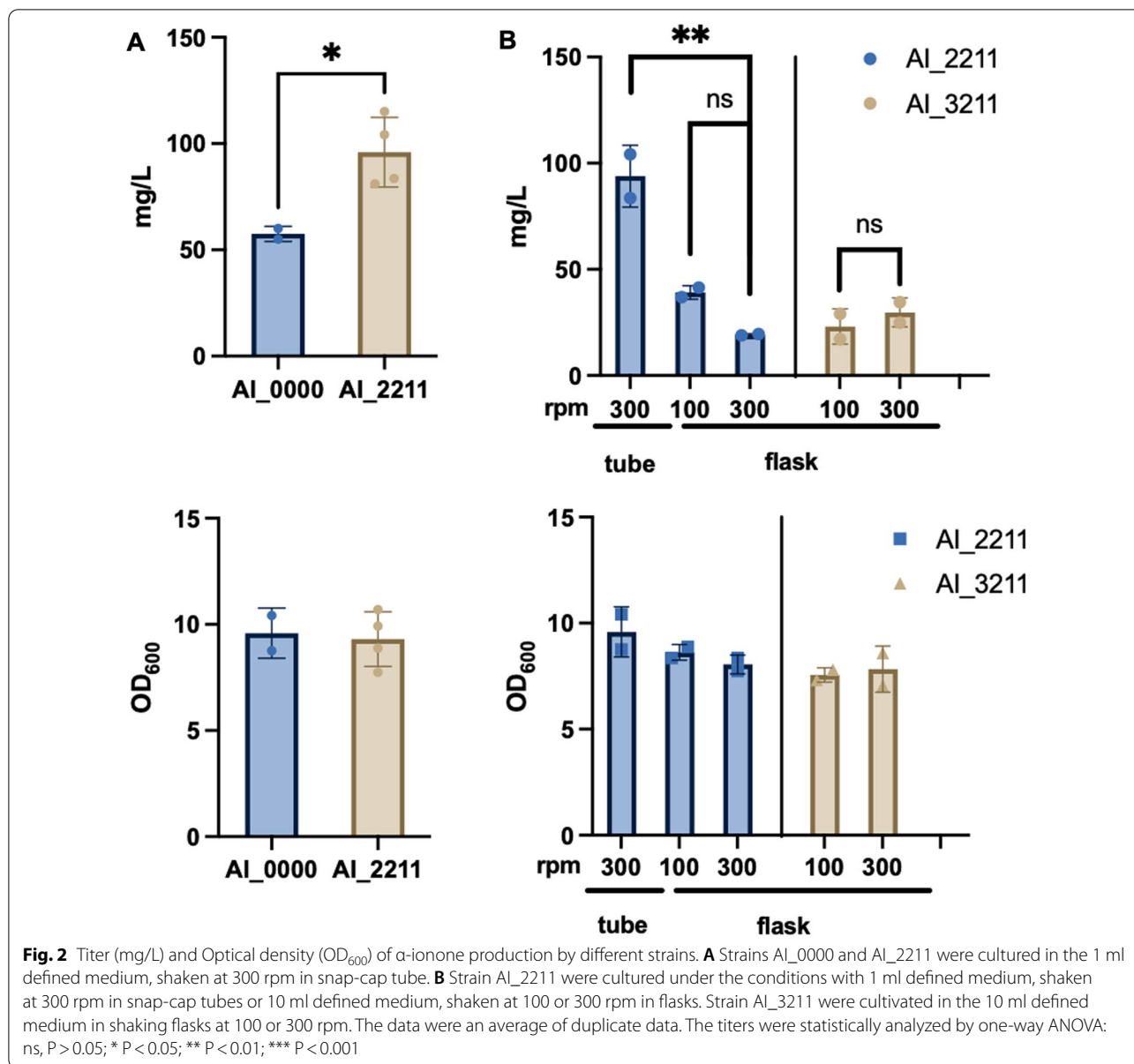
that AhpC/F could effectively remove  $H_2O_2$  in our bacterial strain and hence increased the ionone titer (strain AI\_2218, Fig. 1). The strain overexpressing AhpC/F was successfully scaled up in 5L bioreactors and achieved approximately 700 mg/L  $\alpha$ -ionone, the highest titer in literature.

## Results

### Oxygen sensitivity of new strain: AI\_2211

Previously, we constructed a modular biosynthetic pathway for  $\alpha$ -ionone production in *E. coli* [4]. This biosynthetic pathway consists of 4 modules: (I) an upstream mevalonate pathway; (II) a downstream mevalonate pathway; (III) a lycopene pathway; and (IV) an  $\alpha$ -ionone pathway (Fig. 1). Based on our modification of this biosynthetic pathway, we named the  $\alpha$ -ionone producing strain AI\_ABCD (Additional file 1). To improve the production of  $\alpha$ -ionone, we overexpressed an additional copy of CCD1 in the first module to enhance the  $\epsilon$ -carotene conversion to  $\alpha$ -ionone and the expression levels of pathway genes were re-optimized, namely, strain AI\_2211 (Fig. 1) [7]. We first tested the strain in snap-cap tubes (with the shaking speed of 300 rpm) and the strain AI\_2211 produced 96 mg/L of  $\alpha$ -ionone, which is >65% higher than our previous best strain AI\_0000 (Fig. 2A). However, the titer dropped to 19.3 mg/L when we tested the strain in flasks (with the shaking speed of 300 rpm) (Fig. 2B). In flasks,  $\alpha$ -ionone production increased from 19.3 to 39.2 mg/L while reducing the shaking speed from 300 to 100 rpm (Fig. 2B). This indicated that the productivity of strain AI\_2211 was highly sensitive to the change of shaking speed. We wondered if the observed negative effect of shaking speeds on  $\alpha$ -ionone production was due to an additional copy of the CCD1 gene on the plasmids present in strain AI\_2211. To test this hypothesis,



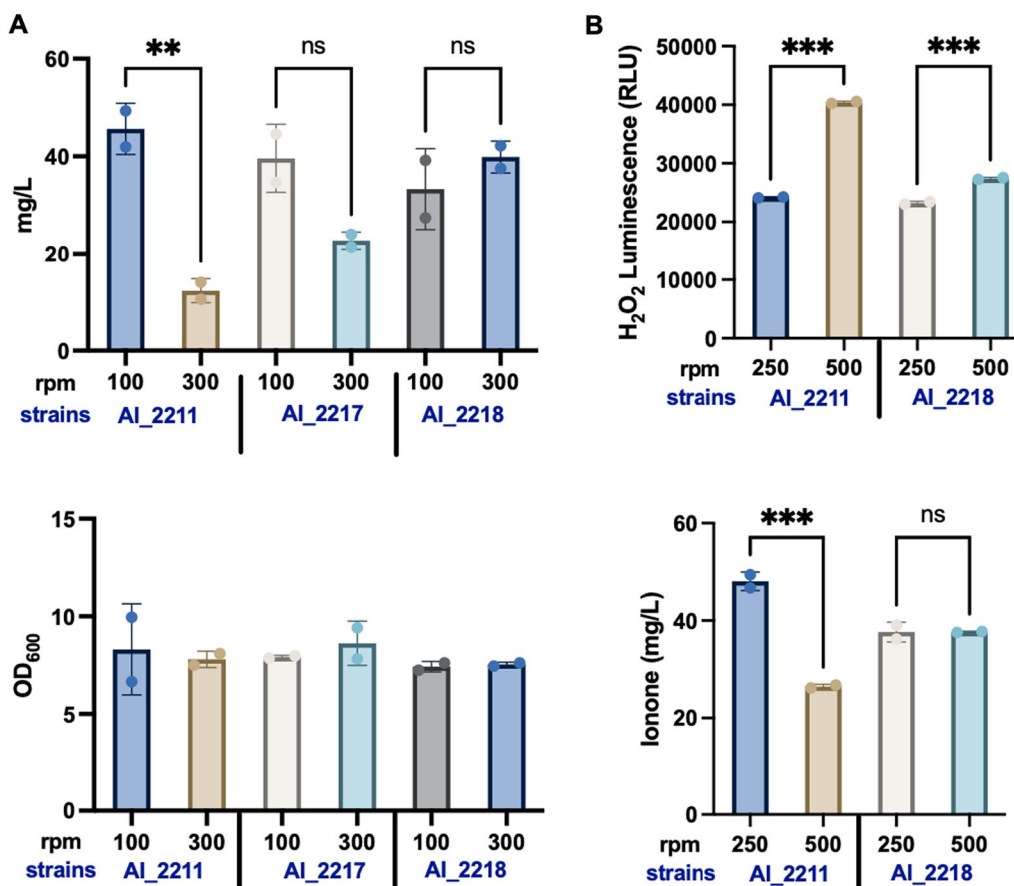


we removed the extra CCD1 gene while keeping all the remaining genes identical to strain AI\_2211 in obtaining strain AI\_3211 (Additional file 1). We compared these two strains at shaking speeds of 100 rpm and 300 rpm in flasks. Interestingly, strain AI\_3211 produced a slightly higher amount of α-ionone at 300 rpm (30 mg/L) compared to at 100 rpm (23 mg/L), suggesting the strain was less sensitive to the change of shaking speed (Fig. 2B). In contrast, strain AI\_2211 produced around a twofold higher amount of α-ionone at 100 rpm compared to 300 rpm (Fig. 2B). Higher shaking speeds contributed to higher amounts of dissolved oxygen and potentially higher oxidative stress in flasks. Hence, we hypothesized

that this phenomenon might be attributed to the generation of reactive ROSs, especially H<sub>2</sub>O<sub>2</sub>.

**H<sub>2</sub>O<sub>2</sub> production of in vivo overexpression of catalase genes; catalase G (katG): strain AI\_2217 and alkyl hydroperoxide reductase (ahpC/F): strain AI\_2218**

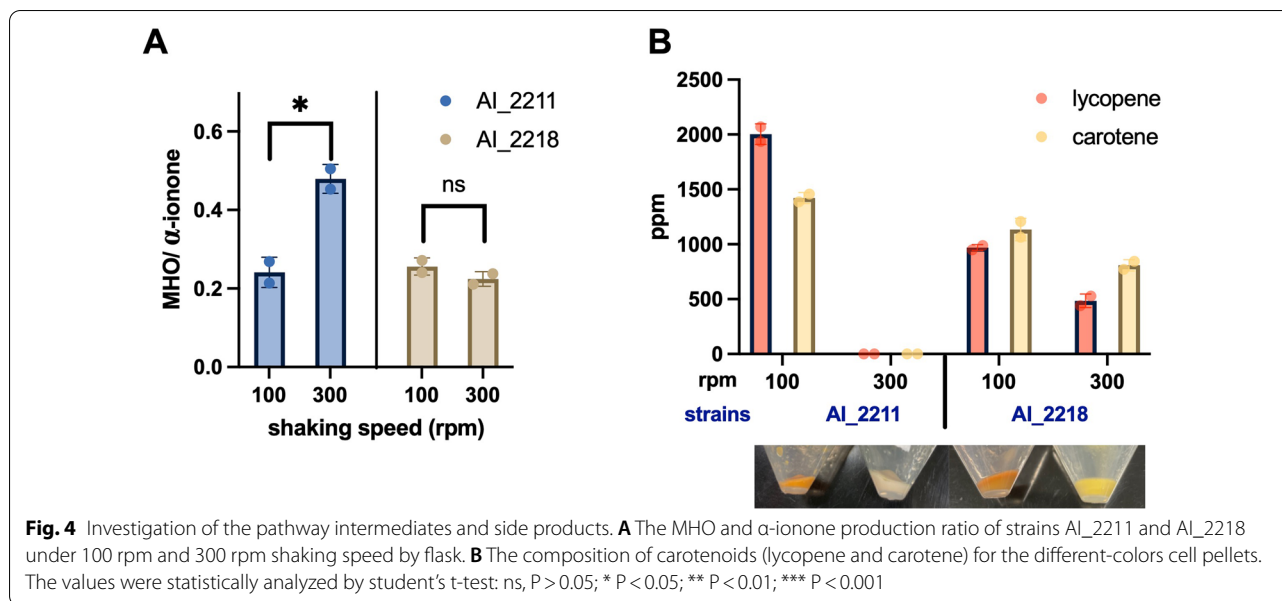
To test our hypothesis, we overexpressed *katG* and *ahpC/F* in strain AI\_2211 to obtain strain AI\_2217 and AI\_2218, respectively (Additional file 1). We then compared α-ionone titers of 3 different strains (AI\_2211, AI\_2217, and AI\_2218). We found strain AI\_2218 yielded higher α-ionone titers at higher shaking speeds (300 rpm vs 100 rpm). However, strain AI\_2217 exhibited the same



**Fig. 3** In vivo overexpression of *katG* and *ahpC/F* and ROS-Glo™ Assay signals from H<sub>2</sub>O<sub>2</sub> production by strains. **A** Strains AI\_2211, AI\_2217, and AI\_2218 were cultivated in the 10 ml defined medium with 10 ml dodecane in shaking flasks at 100 rpm and 300 rpm. The data were an average of duplicate data. **B** α-Ionone titers of AI\_2211 and AI\_2218 under 250 rpm or 500 rpm shaking speed by RTS-1C (Personal bioreactor) and after incubation 1.5 h, 100 μL of each testing strains AI\_2211 and AI\_2218 mixed culture plated in a 96-well white cell culture plate and 100 μL of ROS-Glo™ Detection Solution was added to the wells. Luminescence was determined with a GloMax® Multi + Luminometer. The average relative light unit (RLU) and standard deviation of quadruplicate samples were calculated. The titers and luminescence values were statistically analyzed by one-way ANOVA: ns, P > 0.05; \* P < 0.05; \*\* P < 0.01; \*\*\* P < 0.001

trend as strain AI\_2211 with about a twofold higher yield of α-ionone at 100 rpm compared to that at 300 rpm (Fig. 3A). The results showed that α-ionone titers of strains AI\_3211 and AI\_2218 were positively correlated with shaking speed and relatively insensitive to the change of shaking speed, while those of strains AI\_2211 and AI\_2217 were negatively correlated with shaking speed and displayed higher sensitivity towards shaking speed change (Figs. 2B and 3A). Furthermore, we measured H<sub>2</sub>O<sub>2</sub> production using the ROS-Glo™ H<sub>2</sub>O<sub>2</sub> Assay with strains AI\_2211 and AI\_2218 in a 1 ml defined medium. The assay was conducted at shaking speeds of 250 (lower shaking speed) and 500 (higher shaking speed) rpm by RTS-1C to save ROS-Glo™ detection reagents (a mini bioreactor with better-shaking speed control) instead of in flasks. Our results indicated H<sub>2</sub>O<sub>2</sub> concentration to be about 40,000 relative light unit (RLU)

for strain AI\_2211 shaken at 500 rpm (higher shaking speed), which was 1.6-fold higher than that of strain AI\_2211 shaken at 250 rpm (lower shaking speed) and that of strain AI\_2218 shaken at both speeds (Fig. 3B). The measurement of H<sub>2</sub>O<sub>2</sub> concentration demonstrated that at high agitation rates, strain AI\_2211 was associated with more oxidative stress by H<sub>2</sub>O<sub>2</sub>. Moreover, it also proved that strain AI\_2218 eliminated H<sub>2</sub>O<sub>2</sub> efficiently because of *ahpC/F* overexpression. Also, the α-ionone production was inversely correlated with the H<sub>2</sub>O<sub>2</sub> accumulation for strain AI\_2211, whereas similar α-ionone titers were obtained for strain AI\_2218 when H<sub>2</sub>O<sub>2</sub> concentration remained low (Fig. 3B). This suggests that indeed H<sub>2</sub>O<sub>2</sub> negatively affected α-ionone biosynthesis.



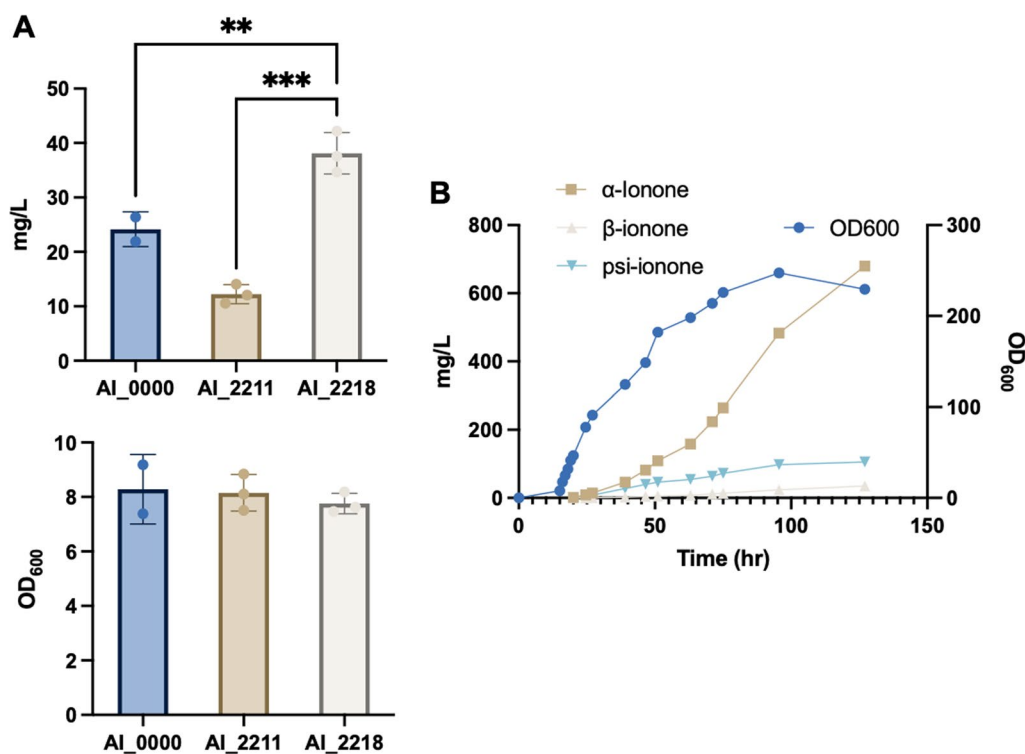
#### 6-Methyl-5-hepten-2-one (MHO) production in strain AI\_2211 and strain AI\_2218 under different shaking speed conditions

Next, we would like to examine how  $H_2O_2$  affected the  $\alpha$ -ionone pathway and further decreased the production of  $\alpha$ -ionone in strain AI\_2211. From previous experiments, we observed that the pellet colors of strain AI\_2211 were orange and white at shaking speeds of 100 rpm and 300 rpm, respectively. Naturally-occurring lycopene is red and  $\epsilon$ -carotene is yellow [8]. Thus, we postulate that the  $H_2O_2$  might degrade some intermediates of the pathway, such as lycopene and  $\epsilon$ -carotene; this would reduce the pathway flux for  $\alpha$ -ionone production. From the experiment with strains AI\_2211 and AI\_2218 inoculated at shaking speeds of 100 rpm and 300 rpm, we noted the presence of 6-Methyl-5-hepten-2-one (MHO), which is an oxidative degradation product of lycopene [9]. We compared the production of MHO with  $\alpha$ -ionone in different cells. The MHO to the  $\alpha$ -ionone ratio of strain AI\_2211 at 300 rpm was about 0.5 which was two times higher than in all other tests done (around 0.2–0.3) (Fig. 4A). These results indicated that the high shaking speeds led to the high  $H_2O_2$  accumulation which degraded the lycopene to MHO in strain AI\_2211, and the reduced supply of lycopene further contributed to the decrease in  $\alpha$ -ionone production (Fig. 1). Moreover, carotenoid degradation can also be proven from the colorless pellet of strain AI\_2211 shaken at 300 rpm (compared to the orange pellet of strain AI\_2211 shaken at 100 rpm and the yellow pellet of strain AI\_2218 shaken at 300 rpm) (Fig. 4B). For strain AI\_2211 at 300 rpm, we couldn't

detect any peak of lycopene and  $\epsilon$ -carotene, consistent with its colorless pellets. At 100 rpm, ~2000 ppm lycopene and 1400 ppm  $\epsilon$ -carotene were produced in strain AI\_2211. For strain AI\_2218 at both 100 and 300 rpm, we detected the intracellular  $\epsilon$ -carotene and lycopene, although the contents were a bit less than that in strain AI\_2211 at 100 rpm (Fig. 4B).

#### Strain AI\_2218, bioreactor fermentation for $\alpha$ -ionone production

Before scaling up in a 5 L bioreactor, we compared strains AI\_0000, AI\_2211, and AI\_2218 in flasks at 300 rpm to confirm that strain AI\_2218 can produce higher  $\alpha$ -ionone titers (Fig. 5A). Indeed, strain AI\_2218 gave the highest  $\alpha$ -ionone yield (5.0 mg/L/OD) as compared to strain AI\_0000 (3.0 mg/L/OD) and strain AI\_2211 (1.5 mg/L/OD) (Additional file 2). Although strain AI\_2211 produced the highest amount of  $\alpha$ -ionone under 1 ml defined medium at 300 rpm shaking speed (11.4 mg/L/OD) (Additional file 2), due to its extremely high sensitivity towards oxygen, scaling up using strain AI\_2211 is very challenging. In comparison, strain AI\_2218 had higher  $\alpha$ -ionone yield and higher robustness as less sensitive to oxygen, which is more promising for scaling up. The 5 L bioreactor experiment was thus subsequently performed with strain AI\_2218, yielding approximately 700 mg/L  $\alpha$ -ionone in 127 h (Fig. 5B), which is about 75% higher than a recent achievement in *Yarrowia lipolytica* [10].



**Fig. 5** Fed-batch fermentation for  $\alpha$ -ionone production. **A** Compare  $\alpha$ -ionone titer and OD<sub>600</sub> by different strains: AI\_0000, AI\_2211, and AI\_2218. All done in 10 ml defined medium with 10 ml dodecane by flask under 300 rpm shaking speed. The titers were statistically analyzed by one-way ANOVA: ns,  $P > 0.05$ ; \*  $P < 0.05$ ; \*\*  $P < 0.01$ ; \*\*\*  $P < 0.001$ . **B** The fed-batch fermentation of strain AI\_2218. Time course profiles of ionone production and cell growth (OD<sub>600</sub>). At the endpoint of 127 h, final OD<sub>600</sub> was 229.3, and the titers of  $\alpha$ -,  $\beta$ - and  $\psi$ -ionone were 679.9, 35.2 and 105.8 mg/L, respectively

## Discussion

In this study, we improved  $\alpha$ -ionone titer with strain AI\_2211 by reengineering the biosynthetic pathway and further overexpressing the CCD1 encoding gene. CCD enzymes have been found to be a limiting step in both *E. coli* and yeasts to produce apocarotenoids [10, 11], and their low activities often limit the bioproduction of apocarotenoids [4]. However, our study here indicates that expressing too much CCD1 has a disadvantage that the strain suffers from low stability and high sensitivity to oxygen. This low robustness severely impacted its scaling up; while scaling up from 1 mL test tubes to 10 mL shake flasks, the ionone production dropped significantly from 96 to 19.3 mg/L. Furthermore, we found that lowering the shaking speed from 300 to 100 rpm could partially alleviate the problem. Since shaking flasks have relatively higher oxygen supply than test tubes due to wider space and higher shaking speed leads to higher oxygen supply, we hypothesized that oxidative stress induced by high oxygen supply could be the reason for the drastically decreased yield of strain AI\_2211 in flasks (Fig. 2B). Moreover, we showed that the oxidative stress displayed in strain AI\_2211 was due to the additional copy

of CCD1. Oxidative stress in cells are often the result of ROSs accumulation, which can damage intracellular components (such as lipids, proteins, and DNA) [12]. This led us to speculate that the elevated CCD1 activity could be positively correlated with the accumulation of ROSs [13]. H<sub>2</sub>O<sub>2</sub> is a major ROS formed during the aerobic respiration process. Our results further indicated that strain AI\_2211 produced higher concentrations of H<sub>2</sub>O<sub>2</sub> at higher shaking speeds (Fig. 3B), which validated our hypothesis that overexpressing too much CCD1 can lead to higher oxidative stress to the cells and reducing the strain robustness. This could be due to the reduction of O<sub>2</sub> to H<sub>2</sub>O<sub>2</sub> during CCD1 catalysis, which warrants further studies.

Next, we further confirmed higher amounts of H<sub>2</sub>O<sub>2</sub> led to faster lycopene degradation and produced a higher amount of side products such as MHO (Fig. 4). This finding is rational as lycopene is a potent antioxidant that has many double bonds and is easily oxidized by ROSs including H<sub>2</sub>O<sub>2</sub>. As the direct precursor to  $\epsilon$ -carotene and  $\alpha$ -ionone, lycopene degradation further reduced the carbon flux towards  $\alpha$ -ionone (Fig. 1). To prevent this, we harnessed *E. coli*'s native mechanisms to mitigate

oxidative damage by overexpressing alkyl hydroperoxide reductase (AhpC/F) and the catalase KatG to scavenge excess H<sub>2</sub>O<sub>2</sub> [14]. When the intracellular H<sub>2</sub>O<sub>2</sub> concentration is low in *E. coli*, AhpC/F is critical in eliminating H<sub>2</sub>O<sub>2</sub> [15], but when the intracellular H<sub>2</sub>O<sub>2</sub> level rises to more than 20 μM, the dominant role shifts to KatG [15]. Our data indicated that AhpC/F was more effective than KatG in reducing H<sub>2</sub>O<sub>2</sub> and its overexpression in strain AI\_2218 resulted in higher α-ionone production at 300 rpm in flask (Fig. 3A) which could be because intracellular H<sub>2</sub>O<sub>2</sub> concentration was below 20 μM in our ionone strains.

As compared to strain AI\_2211, strain AI\_2218 has shown improved robustness to oxygen fluctuation and stable α-ionone production in both low and high shaking speeds in flasks. This robustness was successfully translated from 10 mL flasks to 5L bioreactors, in which strain AI\_2218 produced approximately 700 mg/L, the highest titer for α-ionone obtained in microbial cell factories reported to date, paving the way for its commercialization. More importantly, we believe the strategy of mediating oxidative stress is inspiring to the biosynthesis of other commercially important apocarotenoids, such as β-ionone, retinol and crocin, in which oxygenases are also involved similarly to CCD1 here.

We also highlighted that the ionone production of AI\_2218 in flasks (5.0 mg/L/OD) was still much lower than that of AI\_2211 in tubes (11.4 mg/L/OD) (Additional file 2), indicating there are still factors and conditions which we have not explored; identifying these factors and conditions may lead to further increase in α-ionone bioproduction. For instance, in the future, we may further engineer the strain to better balance the CCD1 and AhpC/F activities, so that CCD1 activities are sufficient and H<sub>2</sub>O<sub>2</sub> production is minimized concurrently.

Lastly, our study reiterates the difficulty in scaling up for some high-yield strains from small scale, due to the differences among tubes, flasks and bioreactors. For example, strain AI\_2211 has a very high α-ionone yield in tubes but cannot be scaled up even to 10 mL flasks. As such, we may face a trade-off between yields and robustness. To guarantee stable outputs and product quality in industrial production, we may have to choose a strain with higher robustness but a relatively lower yield such as strain AI\_2218.

## Conclusion

CCD1 is known to be the limiting enzyme for α-ionone biosynthesis. Here, we increased CCD1 activities by introducing an extra copy of CCD1 in a plasmid, which did improve ionone production in shake tubes. However, the increased CCD1 activities also reduced strain stability

and elevated the oxidative stress as shown in the accumulation of higher amount of H<sub>2</sub>O<sub>2</sub>. H<sub>2</sub>O<sub>2</sub> accelerated the degradation of lycopene (the precursor to α-ionone) and reduced the flux towards α-ionone while scaling up in flasks. Therefore, we overexpressed *ahpC/F* which successfully removed H<sub>2</sub>O<sub>2</sub> and prevented the rapid degradation of lycopene, leading to a further increase in α-ionone titer and higher robustness in flasks. To the best of our knowledge, this is the first study that investigated oxidative stress induced by CCD1 and its effect on α-ionone production, which is inspiring to the biosynthesis of other commercially important apocarotenoids, such as β-ionone, retinol and crocin. Finally, our best strain produced 700 mg/L (here, the titre was calculated based on the final volume of aqueous phase) α-ionone in a 5 L bioreactor, which was the highest in the literature, paving the way for its commercialization.

## Methods

### Bacteria strains, plasmids, and oligonucleotides

The bacterial strains and plasmids used in this study are listed in Additional file 1. The specific oligonucleotides used for PCR amplification were synthesized by Integrated DNA Technologies (IDT) and listed in Additional file 3. We constructed Modules 4–7 (p15A-amp-ΔN50LsLCYe-OfCCD1-trxA (TM1) with three mutations of OfCCD1 active site loop, adding *katG*) and 4–8 (p15A-amp-ΔN50LsLCYe-OfCCD1-trxA (TM1) with three mutations of OfCCD1 active site loop, adding *ahpC/F*). The backbone was amplified with Module 4–1 as a template and the genes of the *katG* and *ahpC/F* were amplified from *E. coli* BL21. Cloning was performed using the iProof™ High-Fidelity DNA Polymerase (BIO-RAD).

### Media and culture conditions

All the cells were grown in LB media [16]. For the production test, a chemically defined auto-induction medium was used, which contained 2 g/L glucose and 8 g/L glycerol, 2 g/L ammonium sulfate, 4.2 g/L KH<sub>2</sub>PO<sub>4</sub>, 11.24 g/L K<sub>2</sub>HPO<sub>4</sub>, 1.7 g/L citric acid, 0.5 g/L MgSO<sub>4</sub>, and 10 mL/L trace element solution. The trace element solution (100 x) contained 0.25 g/L CoCl<sub>2</sub>·6H<sub>2</sub>O, 1.5 g/L MnSO<sub>4</sub>·4H<sub>2</sub>O, 0.15 g/L CuSO<sub>4</sub>·2H<sub>2</sub>O, 0.3 g/L H<sub>3</sub>BO<sub>3</sub>, 0.25 g/L Na<sub>2</sub>MoO<sub>4</sub>·2H<sub>2</sub>O, 0.8 g/L Zn(CH<sub>3</sub>COO)<sub>2</sub>, 5 g/L Fe(III) citrate, and 0.84 g/L ethylenediaminetetraacetic acid (EDTA) at pH 8.0. The auto-induction medium was supplemented with the appropriate antibiotics (100 mg/L ampicillin, 34 mg/L chloramphenicol, 50 mg/L kanamycin, and 50 mg/L spectinomycin) to maintain corresponding plasmids. Cells were induced by 15 mM lactose [17]. 1% fresh cell culture was inoculated into 1 ml of

auto-induction medium in 14 ml snap cap tubes and 10 ml of auto-induction medium in 100 ml flasks. After induction, dodecane (200  $\mu$ L for the 1 ml culture and 10 ml for the 10 ml culture) was added to the culture to extract ionone, and the cells were incubated at 28 °C for 72 h with a shaking speed of 100 rpm or 300 rpm before harvest.

#### Quantification of $\alpha$ -ionone and 6-Methyl-5-hepten-2-one (MHO)

The  $\alpha$ -ionone, or MHO samples were prepared by diluting 10–50 times of organic layer into 1000  $\mu$ L hexane. Gas chromatography–mass spectrometry (GC–MS) analyses of the samples were performed on an Intuvo 9000 GC system attached with a 5977B MS detector (Agilent Technologies, USA). The system was equipped with a polar DB wax column (polyethylene glycol (PEG); 30 m  $\times$  0.25 mm I.D.  $\times$  0.25  $\mu$ m; Agilent Technologies, USA) and a split injector (split ratio 1:10). The oven program started at 80 °C for 1 min, with temperature increased by 20 °C/min until 130 °C, held for 1.5 min, before being increased by 40 °C/min until 200 °C. This was held for 2 min, before being finally increased by 80 °C/min and maintained at 230 °C for another 2 min. Helium was used as the carrier gas at a constant flow rate of 1.0 mL/min. The Agilent 5977B mass spectrometer was operated in the electron ionization mode at 70 eV with a source temperature of 230 °C, transfer line temperature set at 250 °C, and a scan range of  $m/z$  50–500 in the full scan mode at an acquisition rate of 3.6 scans/s. Methanol was the solvent for the column wash and hexane for the needle wash. The injection volume was 1  $\mu$ L. The ionone concentrations were calculated by interpolating with a standard curve prepared by commercial standards (Sigma-Aldrich Pte Ltd, Singapore). The mass spectrometer was operated in EI mode with a full scan analysis.

#### ROS-Glo™ H<sub>2</sub>O<sub>2</sub> Assay

ROS-Glo (Promega, Madison, WI, USA) assay was used as specified to quantify H<sub>2</sub>O<sub>2</sub> production [18, 19]. *E. coli* strains AI\_2211 and AI\_2218 were inoculated into 1 ml auto-induced R-medium by RTS-1C (Personal Bioreactor, Biosan). Cells were grown to an OD<sub>600</sub> of 1.5–2.0 and then the H<sub>2</sub>O<sub>2</sub> substrate was added. The culture was subsequently incubated for 1.5 h, the cells harvested, and the amount of luciferin precursor produced measured. The H<sub>2</sub>O<sub>2</sub> substrate reacts directly with H<sub>2</sub>O<sub>2</sub> to generate a luciferin precursor. Upon addition of ROS-Glo™ Detection Reagent containing Ultra-Glo™ Recombinant Luciferase and d-Cysteine, the precursor is converted to luciferin by the d-Cysteine, and

the luciferin produced reacts with Ultra-Glo™ Recombinant Luciferase to generate a luminescent signal that is proportional to H<sub>2</sub>O<sub>2</sub> concentration (ROS-Glo™ H<sub>2</sub>O<sub>2</sub> Assay, Promega). 800  $\mu$ L of cells were incubated with 200  $\mu$ L of H<sub>2</sub>O<sub>2</sub> substrate followed by the addition of the ROS-Glo detection reagent. Luminescence corresponding to H<sub>2</sub>O<sub>2</sub> levels was measured using a micro plate reader (Molecular Devices, San Jose, CA, USA).

#### Quantification of carotenoids

Intracellular carotenoids were extracted from cellular pellets according to the previous method [4]. Briefly, 10–50  $\mu$ L bacterial culture was collected and centrifuged. Cell pellets were washed with PBS and were resuspended in 20  $\mu$ L of water, followed by addition of 180  $\mu$ L of acetone. The high performance liquid chromatography (HPLC) method was modified as previously described. Briefly, the analysis employed an Agilent 1260 Infinity LC System equipped with a ZORBAX, Eclipse Plus C18, 4.6  $\times$  250 mm, 5  $\mu$ m column and diode array detector (DAD). Isocratic condition (50% methanol, 48% ethyl acetate, and 2% water) was maintained at 1.5 mL/min for 5 min. The carotenoids were detected at wavelength of 450 nm. Standard curves were generated using commercial standards of  $\epsilon$ -carotene (CaroteNature, Switzerland) and lycopene (Santa Cruz Biotechnology, Dallas, TX).

#### Fed-batch fermentation

The starting medium was a chemically defined medium modified from previous studies [17], which contained 5 g/L of glucose transferred into a 5L bioreactor with an initial working volume of 1.8L. The *E. coli* strain AI\_2218 was inoculated into the sterile defined medium to obtain an initial optical density at 600 nm (or OD<sub>600</sub>) of 0.1. The fermentation was first carried out under the controlled set points of pH, temperature, and dissolved oxygen at 7.0, 37 °C, and 30%, respectively. After inoculation, peristaltic pumping of the feedstock solution (containing 750 g/L glucose and 7.5 g/L MgSO<sub>4</sub>) at 1.62 mL/h flow rate was carried out overnight (~13 h). The pH of the culture was controlled at 7.0 using an alkaline solution (a mixture of 28% ammonium hydroxide and 1 M sodium hydroxide solution; in ratio 1:1 by volume) throughout the experiments. The flow rate of feedstock was changed to an exponential feeding rate after 13 h, cells were induced by 0.1 mM Isopropyl  $\beta$ -D-thiogalactopyranoside (IPTG) when OD<sub>600</sub> reached about 40.0 and 700 mL of sunflower oil as an extractant was



then added to the bioreactor. Dissolved oxygen was subsequently lowered to 15% and the flow rate of the feedstock was kept constant at 15.6 mL/h after induction.

#### Abbreviations

CCD1: Carotenoid cleavage dioxygenase 1; H<sub>2</sub>O<sub>2</sub>: Hydrogen peroxide; ROS: Reactive oxygen species; *ahpC/F*: Alkyl hydroperoxide reductase; MHO: 6-Methyl-5-hepten-2-one.

#### Supplementary Information

The online version contains supplementary material available at <https://doi.org/10.1186/s12934-022-01968-1>.

**Additional file 1.** Strains and plasmids used in the study.

**Additional file 2.** Content (Titer/OD600) of different  $\alpha$ -ionone producing strains.

**Additional file 3.** Oligonucleotides used for PCR amplifications.

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#### Author contributions

XXC and CQZ conceived the study and supervised the work. CNH and XHL performed and constructed the  $\alpha$ -ionone strains AL\_2211, AL\_3211, AL\_2217 and AL\_2218, quantified  $\alpha$ -ionone and MHO, and performed ROS-Glo™ H<sub>2</sub>O<sub>2</sub> Assay. CNH and XHL collected and analyzed the data. LO and CCL performed the fed-batch fermentation, collected and analyzed the data. CNH and CQZ drafted the manuscript. XXC and CQZ reviewed and revised the manuscript. All authors read and approved the final manuscript.

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#### Availability of data and materials

All the data analyzed in this study are included in this manuscript.

#### Declarations

##### Ethics approval and consent to participate

Not applicable.

##### Consent for publication

Not applicable.

##### Competing interests

The authors declare that they have no competing interests.

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